Current Chemistry Letters 2 (2013) 57–68

Contents lists available at Growing Science

Current Chemistry Letters

homepage: www.GrowingScience.com/ccl

Central composite design for the optimization of removal of the azo dye, Methyl Red, from waste water using Fenton reaction

Mahsa Azami* , Morteza Bahram and Sirous Nouri

Department of Chemistry, Faculty of Science, Urmia University, Urmia, Iran

CHRONICLE	ABSTRACT
Article history: Received October 26, 2012 Received in Revised form March 10, 2013 Accepted 15 March 2013 Available online 15 March 2013 Keywords: Design of experiments Methyl red Degradation Fenton reaction	In this study the degradation of an azo dye, Methyl Red, which is used in textile industry, using Fenton reaction was studied and optimized by a chemometrics method. Fenton oxidation is one of the Advanced Oxidation Processes (AOPs), in which hydroxyl radicals are generated from Fenton's reagents (Fe ²⁺ , H ₂ O ₂). The effects of various experimental parameters in this reaction were investigated using Central Composite Design (CCD) method. The experimental design was done at five levels of operating parameters. 28 experiments, with 4 factors and 5 levels for each factor were designed. These factors (or variables) include $[Fe^{2+}]$, $[H_2O_2]$, [oxalate] and the reaction time. A full-quadratic polynomial equation between the percentage of dye degradation (as the response) and the studied parameters was established. After removing the non- significant terms from the model, response surface method was used to obtain the optimum conditions. The optimum ranges of variables were: $0.1 - 0.4$ mM for $[Fe^{2+}]$, 13.5-22 mM for $[H2O2]$, 1.5-2 mM for [Oxalate], and 115-125 min for the reaction time. Also the results of extra experiments showed that these optimized values can be used for real samples and yield to high values for the response.

© 2013 Growing Science Ltd. All rights reserved.

1. Introduction

1.1. AZO DYES

 There are many branches of industries, *i.e.* textile, painting, leather, printing, paper production, food technology, photography etc., which use various colorants (synthetic dyes)^{1,2}. The release of such coloured wastewaters into the environment is a dramatic source of aesthetic pollution, eutrophication and perturbations in aquatic life³. The presence of these synthetic dyes can also make problems within the use and reuse of water streams, distribute the beautiful appearance of waters and

 $*$ Corresponding author. Tel: +98-8318236845 E-mail addresses: mahsa.azami@gmail.com (M. Azami)

© 2013 Growing Science Ltd. All rights reserved. doi: 10.5267/j.ccl.2013.03.003

also reduce the effectiveness of microbial waste water treatment because they can be toxic to microorganisms.

Dyes in effluents absorb and scatter sunlight, which is essential for algae growth. These effluents are threat to the ecosystems due to its toxicity and resistance to destruction by biological treatment methods¹ Dyes which release in wastewater should be seriously concerned because they give an undesirable color to the waters and also in some cases are themselves harmful compounds and can lead to generate harmful by-products through various reactions taking place in the waste phase⁴.

There is a wide variety of dyes on the market for various applications. Dyes can be classified as azo dyes, triaryl methane dyes, anthraquinone dyes, heterocyclic dyes, and phthalocyanine dyes, depending on their chemical structures. Dyes can also be characterized according to their application method as reactive dyes, direct dyes, acidic dyes, disperse dyes, and cationic dyes⁵.

Azo dyes, constituting the largest class among the synthetic colorants, are considered as the widespread environmental pollutants associated with many important industries such as textile, food colorants, printing and cosmetic manufacturing. It is estimated that approximately 800,000 t of dyes are produced annually worldwide and about 50% of them are azo dyes⁶. Azo dyes are the largest class of dyes commercially used in the textile industries. Most of these compounds are highly resistant to microbial attack, and are, therefore, hardly removed from effluents by conventional biological wastewater treatments, such as activated sludge⁷. The release of azo dyes into the environment is of great concern, due to coloration of natural waters and toxicity, mutagenicity, and carcinogenicity of the dyes and their toxic biotransformation products⁸.

Methyl red, also called C.I. Acid Red 2, is an indicator dye that turns red in acidic solutions. It is an azo dye, and is a dark red crystalline powder. Methyl red is a pH indicator; it is red in pH under 4.4, yellow in pH over 6.2, and orange in between, with a pKa of 5.1.

This dye is also used in textile industries and has the maximum of absorbance at λ max=432nm. Some of Methyl red's characteristics are shown in **Table 1**. Methyl Red is a harmful compound that exists in textile waste waters and has various harmful effects on human beings. For example it may cause eye or skin irritation, or inhalation may cause gastrointestinal irritation with nausea, vomiting, and diarrhea^{9,10}.

Name	Structure	Molecular weight (g/mol)	Chemical Formula
Methyl Red	$- N = N$ CH_1N- H-	269.31	$C_{15}H_{15}N_3O_2$

Table 1. Some characteristics of Methyl Red.

1.2. Advanced Oxidation Processes

To avoid the dangerous accumulation of dyes in the environment, there is a need to develop effective methods for the degradation of such organic pollutants, either to less harmful compounds or, more desirable, to their complete mineralization¹¹.

There are many different technological processes such as adsorption¹, biodegradation, chemical methods (e.g. chlorination and ozonation), electrocoagulation, electrochemical reduction and oxidation, indirect Electro-oxidation with strong oxidants and photocatalytic degradation, which can be used to treat the waste waters including these synthetic dves^{5,12}.

 In recent years, Advanced Oxidation Processes (AOPs) have attracted attentions for the destruction of these dyes. In AOPs methods, highly reactive hydroxyl radicals, which have one unpaired electron and are very strong oxidizing agents are produced.

 Fenton's oxidation is one of the AOPs methods, in which hydroxyl radicals are generated from Fenton's reagents¹. Fenton reaction is already in use for industrial wastewater purification processes. It is well-known that, the most important characteristic of heterogeneous Fenton processes is the formation of OH radicals, which are highly oxidative, nonselective, and able to decompose many organic compounds. It is also well-accepted that the advantages of heterogeneous Fenton processes are complete mineralization of organic compounds at ambient temperature and easy separation of the heterogeneous catalysts from the treated wastewater. Because of these advantages, a lot of effort has been made in developing heterogeneous Fenton catalysts containing $Fe²⁺$ ions. The Fenton system uses ferrous ions as catalysts that react with hydrogen peroxide, producing hydroxyl radicals with powerful oxidizing abilities ⁵.

 Generated hydroxyl radicals may then react with ferrous ions, for instance, to form ferric ions, or with the organics. The oxidation products are usually low molecular weight compounds that are often more easily biodegradable or, in some instances, the organic compounds reduced to carbon dioxide and water, among other inorganics 13 .

 The Fenton reaction has many various advantages in the degradation of pollutants, for example its reagents are environmentally safe, cheap and easy to obtain and use. The appropriate pH range for this reaction is 2.0–4.0 and the best pH is $3^{14, 15}$.

 As mentioned above, the Fenton reaction is used for the treatment of azo dyes wastewaters. This reaction can be effective on the degradation of so many azo dyes. The rate of OH generation and the characteristics of these dyes can influence on the percentage of decolorization¹⁶.

So it is obvious that the concentration of iron salt and H_2O_2 have an important effect on the dye removal percentage. In addition, in this study the salt of sodium oxalate is also used to catalyze the removal reaction.

1.3. Optimization

 Optimizing refers to improving the performance of a system, a process, or a product in order to obtain the maximum benefit from it. The term *optimization* has been commonly used in analytical chemistry as a means of discovering conditions at which a procedure produces the best possible response 17.

 In order to optimize the effective variables on decolourisation of Methyl Red, two methods can be used: one-variable-at-a-time method and experimental design techniques. In the first method it is necessary to do many experiments, spend much time and materials.

 There is also a premier problem with this method. Here the interactions between the parameters are ignored and this can lead to incorrect optimized values for the variables and after doing many experiments we cannot claim that the best results are obtained. Therefore, it is obvious that a reliable and trusty method is required to gain the true optimized values. The experimental design is a method which can lead to this goal¹⁸⁻²⁰.

 Experimental design is used to decide which factors influence on the properties of the chemical process or desirable product. Response Surface Methodology (RSM) is a statistical method being useful for the optimization of chemical reactions and/or industrial processes and widely used for experimental design .Whenever multiple system variables may influence the outputs; RSM can be utilized to assess the relationship between dependent (response) and independent variables as well as to optimize the relevant processes^{21,22}. RSM employs a low-order polynomial equation in a predetermined region of the independent variables, which are later on analyzed to locate the optimum values of independent variables to obtain the best (highest) response. Process optimization by RSM is faster for gathering experimental research results than the rather conventional, time consuming onefactor-at-a-time approach $^{23, 24}$.

 In this research, finding optimal conditions for effective factors on degradation of Methyl Red, by Fenton reaction using an experimental design method (Central Composite Design (CCD)) was investigated.

2. Experimental

2.1. Instruments

 The solutions were shaked by a MTOPO magnetic stirrer model MS3300 and the absorbance of the solutions were measured by a PG-mode T80 UV-Vis double-beam spectrophotometer (Japan) utilizing a 1-cm quartz cell. Variation of solution pHs was measured by a pH-meter BEHINEH (UK).

2.2. Reagents

Methyl Red (M_w = 269.31 gr/mol), FeSO₄.7H₂O (M_w = 278 gr/mol), H₂O₂ (a=30% v/v, d=1.11 kg/m³) and Na₂C₂O₄ (M_w= 134 gr/mol), were used in analytical grade (Merck) and all of the solution were prepared with fresh distilled water.

The solution of Fe^{2+} ion was prepared several times during a day and was used immediately to prevent the exchange of Fe^{2+} ion to Fe^{3+} ion.

To adjust the final pH of the solutions, the solutions of H_2SO_4 (0.01M) and NaOH (0.01M) were prepared and used.

2.3. Statistical Software

 Essential Regression and Experimental Design for Chemists and Engineers (EREGRESS), as MS Excel Add-In software, was used to design the experiments and to model and analyze the results.

2.4. Design of Experiments (DOE)

 By using CCD method, 28 experiments (including 4 repetitions at central point) were designed. The factors (variables) were: $[Fe²⁺], [H₂O₂],$ [oxalate] and the reaction time. Although the initial concentration of Methyl Red might be important, but as mentioned, this factor was spotted at the constant value of 0.015 mM. This value for the dye concentration was selected from calibration curve of Methyl Red (the middle point of the linear range in spectrophotometeric determination). For each factor, 5 levels were defined. These values are coincided on the codes: -2 , -1 , 0 , $+1$ and $+2$ and are shown in **Table 2**.

Variable	Name	$Low(-2)$	$\overline{}$			$High(+2)$
F1	/mM Fe^2		25	0. 5		
F2	$[H_2O_2]$ /mM		5.5		16.5	າາ
F3	[Oxalate]/mM		U.S		$\cdot \cdot$	
F4	Time/min				Q4	

Table 2. The variables and values used for CCD

2.5. Preparing the Solutions

At first, it is necessary to find the linear range of Methyl Red as its calibration curve. The calibration curve represents the absorbance values versus concentration values. A spectrum of a solution of Methyl Red which is taken in visible area, shows the maximum wavelength of this dye at 432 nm (Figure 1). Then, several samples with definite concentrations were made and their absorbencies were measured at 432 nm and the linear range of Methyl Red in spectrophotometric detection was specified (Figure 2). A concentration in middle points of this curve was selected and used for the preparing the dve solution in all experiments (0.015 mM) .

Fig 2. The calibration curve of Methyl Red (432 nm)

According to Table 3, in each experiment, two solutions are needed; A blank solution and a sample solution. The concentration of Methyl Red, H_2O_2 , Fe^{2+} and oxalate are extracted from the Table of DOE (Table 2 and Table 3).

The pH of solution was adjusted in 3.5, using H_2SO_4 (0.01M) and NaOH (0.01M), because the appropriate pH for the Fenton reaction is in the range of 3-5. For each reaction, also a blank sample was prepared which was including the same concentration of Methyl Red and Fe^{2+} , but without H_2O_2 and oxalate ions. The aim of preparing blank solution for each experiment is to consider the effect of passing the time on spontaneously probable degradation of Methyl Red. Also the aim of adding the Fe^{2+} in blank solution is to neutralize the eventual effect of Fe^{2+} 's absorption on the absorption of main solution. These samples were shacked with a magnetic stirrer during reaction.

After the prescribed needful time for each reaction (Table 3), the absorbance of these two solutions were measured with the Uv-Vis spectrophotometer.

3. Results and Discussion

3.1. Data Analysis

After doing the experiments, the percentage of dye degradation for each experiment was calculated from Eq. (1) , which was spotted as the response.

$$
\% \text{ degradation} = \left[1 - \left(\frac{\text{sample absorbance}}{\text{blank absorbance}} \right) \right] * 100 \tag{1}
$$

Table 3 shows the percentage of dye degradation for each experiment. Among these 28 experiments, 4 experiments were repetition of central point (numbers 5, 15, 20, 28). These are the experiments in which, all of the factors are in the centric point of their values. Closeness of the responses of these 4 experiments can be a sign of the accuracy of the experiment process. The relation between the collected response and the variables conforms from the following polynomial equation – a full quadratic model- $(Eq. (2))$:

62

Response =
$$
b_0 + b_1 * F_1 + b_2 * F_2 + b_3 * F_3 + b_4 * F_4 + b_5 * F_1 * F_1 + b_6 * F_2 * F_2 + b_7 * F_3 * F_3
$$

+ $b_8 * F_4 * F_4 + b_9 * F_1 * F_2 + b_{10} * F_1 * F_3 + b_{11} * F_1 * F_4 + b_{12} * F_2 * F_3 + b_{13} * F_2 * F_4 + b_{14} * F_3 * F_4$ (2)

In this equation F1, F2, F3 and F4 show the variables and the b_0-b_{14} are the coefficient values obtained by multiple linear regression (MLR).

Run	radic 3. The coucul values designed by CCD and responses $[Fe2+]$	$[H_2O_2]$	[Oxalate]	Time	% Degradation
$\mathbf{1}$	-1	-1		-1	70.10
$\overline{2}$	1			1	60.53
$\overline{\mathbf{3}}$	-1		1	-1	83.09
$\overline{4}$	1	1	-1	-1	49.03
5	$\mathbf{0}$	$\mathbf{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	60.00
6	-1	-1		1	70.75
$\overline{7}$	$\mathbf{1}$	$\mathbf{1}$	$\mathbf{1}$	-1	71.20
$8\,$	θ	$\boldsymbol{0}$	-2	$\boldsymbol{0}$	39.24
9	$\mathbf{1}$	-1	-1	-1	39.57
$10\,$	$\mathbf{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	$\overline{2}$	74.48
$11\,$	-1	$\mathbf{1}$	-1	-1	63.08
12	$\boldsymbol{0}$	$\overline{2}$	$\boldsymbol{0}$	$\boldsymbol{0}$	69.33
13	-1	$\mathbf{1}$	-1	$\mathbf{1}$	79.41
14	-1	-1	-1		70.19
15	$\overline{0}$	$\mathbf{0}$	$\mathbf{0}$	$\mathbf{0}$	61.25
16	$\boldsymbol{0}$	$\boldsymbol{0}$	$\overline{2}$	$\boldsymbol{0}$	69.57
17	$\overline{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	-2	78.42
18	1	-1	-1	1	35.93
19	-2	$\boldsymbol{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	52.15
20	$\boldsymbol{0}$	$\overline{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	61.29
21	$\boldsymbol{0}$	-2	$\boldsymbol{0}$	$\boldsymbol{0}$	50.14
22	-1	$\mathbf{1}$	$\mathbf{1}$	$\mathbf{1}$	77.33
23	$\mathbf{1}$	-1	$\mathbf{1}$	-1	35.16
24	-1	-1	-1	-1	74.38
25	$\overline{2}$	$\boldsymbol{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	14.65
26	1		-1		72.50
27	$\mathbf{1}$	-1	$\,1\,$	$\mathbf{1}$	57.41
28	$\boldsymbol{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	66.67

Table 3. The coded values designed by CCD and responses

 The analysis of variance (ANOVA) and least squares techniques were used to evaluate the statistical significance of the constructed models. The ANOVA consists of determining which factor(s) significantly affect the response, using a Fisher's statistical test (F-test). The significance and the magnitude of the estimated coefficients of each variable and all their possible interactions on the response variable(s) are determined. Effects with a confidence level less than 95% (effects with a p-value higher than 0.05) were discarded and pooled into the error term and a new analysis of variance was performed for the reduced model. Note that the p-value represents a decreasing index of the reliability of a result. Four replicates of the central points were performed to estimate the experimental error. In order to show the fitness of the model, regression coefficient (R) maybe be used. However, the adjusted regression coefficient (R_{adj}) and the prediction regression coefficient (R_{pred}) is better criteria than the absolute regression coefficient (R) . Since the regression coefficient (R) always decreases when a regression variable is eliminated from the model, in statistical modelling the R_{adj} , which takes the number of regression variables into account, is usually selected.

In addition, R_{pred}, which indicates the predictive power of the model, is chosen for the same reason. This parameter was approximated using prediction error sum of squares (PRESS) that is calculated from residuals. So, the regression coefficient (R), adjusted R (R_{adi}), and R for prediction (R_{pred}) together are very convenient to get a quick view of the overall fit and the prediction power of a constructed model²⁵.

In order to find the important factors and build a model to optimize the procedure, we started with a full quadratic model including all terms in (Eq. (2). Then by back elimination process, those terms, which were not significant enough were eliminated from the equation. These terms included the variables or the interactions, which had no effect or very low effect on the response. Each term which its P-value is more than 0.05, is removed from the main equation. The final equation between the response and the variables is shown in Eq. (3). As it is obvious, the concentration of Fe^{2+} ion, and the interactions between the time of Fenton reaction and $Fe²⁺$ ion concentration, oxalate ion concentration and H_2O_2 concentration are significant and have important effects on the percentage of dye removal. Importance of the interactions is shown graphically in **Figure 3**.

% Degradation = b0 + b1*[Oxalate] + b2*Time + b3*[Fe²⁺]*[Fe²⁺] + b4*[Fe²⁺]*[H₂O₂]

Fig. 3. P-values for the terms in reduced polynomial equation

The reduced model using significant linear, quadratic and interaction parameters is defined in the form of above polynomial Eq. (3).

There were not large differences between R values which revealed that the experimental data shows a good fit to the quadratic equations and therefore an acceptable model has been achieved.

3.2. Response surface and selection of optimized values

After the analysis of data, response surfaces of full quadratic model between the response and the variables were depicted. Via these surfaces the relations between the percentage of dye degradation and effective factors are graphically given. These surfaces are shown in **Figure 4**. The optimized

 (3)

ranges for each factor that leads to the best response (the highest percentage of dye degradation), were extracted from these surfaces. The optimized ranges are presented in Table 4.

Variable	Optimized range
$[Fe2+]$ /Mm	$0.1 - 0.4$
$[H_2O_2]$ /mM	13.5-23
[Oxalate $]/mM$	$1.5 - 2$
time]/min	115-125

Table 4. The optimized ranges for 4 variables

Fig. 4. Response surfaces of full quadratic model between percentage of dye degradation and four variables and the interaction between variables

middle point of each optimum range and repeat the experiments at these values. Five repetitive experiments were done in these conditions. As we can see, all the responses were much closed to each other. These results can satisfy that the obtained optimized ranges for this reaction, can lead to high percentages of dye degradation (Table 5). In order to test the accuracy of obtained optimized ranges of variables, it is necessary to select the e
e
o
o

Run	$2 + 7$ TFe	$[H_2O_2]$ /	[Oxalate]/	Time/	Blank	Sample	$\frac{6}{6}$
	/mM	mM	mM	min	Absorbance	Absorbance	Degradation
	0.25	17.75	1.75	120	0.109	0.002	81.65
	0.25	17.75	1.75	120	0.113	0.023	79.64
◡	0.25	17.75	1.75	120	0.115	0.021	81.73
	0.25	17.75	1.75	120	0.110	0.019	82.72
	0.25	17 75	175	120	0.112	0.02	82.14

Table 5. The results of 5 repetitions of optimum conditions

The relative standard deviation (RSD) of these repeated experiments was estimated for the responses to study the precision of the experiments and closeness of the responses (Eq. (4) and Eq. (5)).

$$
s = \sqrt{\frac{(x_i - \overline{x})^2}{n - 1}} = 1.178
$$
\n(4)

 $RSD\% = \frac{s}{\overline{x}} * 100 = 1.44\%$

3.3. Effect of Variables

3.3.1. Effect of [Fe 2+]

With increasing the $[Fe^{2+}]$, an increasing pattern is observed in the percentage of dye degradation; but increasing of the $[Fe^{2+}]$ more than a specific limit, can lead to fix or decrease the percentage of dye degradation. Because with the increasing of $[Fe²⁺]$, an increasing pattern in the OH generation takes place; but the generation of OH in high values, can cause the undesirable reactions between • OH and present H O in the selution OH and present H_2O_2 in the solution.

3.3.2. Effect of [H2O2]

 According to Eq.(C.2) and **Figure 4** it is obvious that there is an interaction between the two factors $[H_2O_2]$ and $[Fe^{2+}]$. In low concentrations of $[Fe^{2+}]$, the $[H_2O_2]$ has no significant effect on the percentage of dye degradation; but with increasing the concentrations of $[Fe^{2+}]$, the effect of $[H_2O_2]$ on the percentage of dye degradation increases (in the form of a linear function).

3.3.3. Effect of [oxalate]

 According to Eq.(C.2) and **Figure 4** there is no interaction between the concentrations of oxalate and other factors. Increasing the concentration of sodium oxalate (as a catalyst), in the form of a linear function, can lead to increasing the percentage of dye degradation.

3.3.4. Effect of time

 According to **Figure 4** two ranges are gained as optimized values for the factor of time (5-10 min and 115-125 min). But it is clear that the second range (115-125 min) has led to higher responses than the other range (5-10 min). Therefore the second range is selected as the best value of time in this reaction.

3.3.5. Interaction parameters

 The Eq. (3) and the response surfaces (**Figure 4**) show that the only important existent interaction between the four effective above factors, is the interaction between [Fe $^{2+}$] and [H₂O₂]. Other interactions were non-significant or low-significant which are discarded from the main equation.

3.4. Real Sample

 After gaining the optimized values for the effective variables and testing them with extra experiments, these experimental qualifications were applied on a real sample which was derivative from the waste water of a local textile factory (Urmia, Iran).

 The results showed that the optimum values have been achieved by CCD and response surface method and that could lead to acceptable responses. **Figure 5** represents the spectrum of real sample before and after treatment by the proposed method. The degradation percentage 76.45 %(using Eq. (B)) was achieved for removal of Methyl Red in real sample.

Fig. 5. Comparison between the spectrum of real sample before using Fenton reaction (blank) and after using Fenton reaction(sample)

4. Conclusion

 In order to obtain the optimized conditions for removal of Methyl Red from a textile wastewater, 28 experiments (including 4 repetitions of central points) using CCD method were designed. The optimized values were: $0.1 - 0.4$ mM for $[Fe^{2+}]$, 13.5-22 mM for $[H_2O_2]$, 1.5-2 mM for [Oxalate], and 115-125 min for the reaction time. These conditions were applied on a real sample and an acceptable response was achieved (76.45 % for dye removal).

References

- 1. Gomathi Devi L., Girish Kumar S., Mohan Reddy K., Munikrishnappa C. (2009) Photo degradation of Methyl Orange an azo dye by Advanced Fenton Process using zero valent metallic iron: Influence of various reaction parameters and its degradation mechanism. *J. Hazard. Mater.*,164, 459-467.
- 2. Hameed B.H., Lee T.W. (2009) Degradation of malachite green in aqueous solution by Fenton process. *J. Hazard. Mater.*,164, 468-72.
- 3. Garc´ıa-Monta˜no J., P´erez-Estrada L., Oller I., Maldonado M. I., Torrades F., Peral J. (2008) Pilot plant scale reactive dyes degradation by solar photo-Fenton and biological processes. *J. Photochem. Photobiol.*, 195, 205-214.
- 4. Khataee A. R., Zarei M., Moradkhannejhad L. (2010) Application of response surface methodology for optimization of azo dye removal by oxalate catalyzed photoelectro-Fenton process using carbon nanotube-PTFE cathode. *Desalination.*, 258,112-119.
- 5. Rodrıguez A., Ovejero G., Sotelo J. L., Mestanza M., Garcıa J. (2010) Heterogeneous Fenton catalyst supports screening for mono azo dye degradation in contaminated wastewaters. *Ind. Eng. Chem. Res*., 49, 498-505.
- 6. Zhou M.*,* He J. (2007) Degradation of azo dye by three clean advanced oxidation processes: Wet oxidation, electrochemical oxidation and wet electrochemical oxidation-A comparative study*. Electrochim. Acta.,* 53,1902-1910.
- 7. Pourbabaee A., Malekzadeh F., Sarbolouki M. N., Mohajeri A. (2005) Decolorization of Methyl Orange (as a model azo dye) by the newly discovered Bacillus Sp*. Iran. J. Chem. Chem. Eng.*, 24, 41-45.
- 8. Jain R., Varshney S., Sikarwar S. (2007) Electrochemical techniques for the removal of Reactofix Golden Yellow 3 RFN from industrial wastes *J. Iran. Chem. Soc..*, 313, 248-253.
- 9. Wang H., Niu J., Long X., He Y. (2008) Sonophotocatalytic degradation of methyl orange by nano-sized Ag/TiO2 particles in aqueous solutions. *Ultrason. Sonochem.*, 15, 387-392.
- 10.Diagne M., Oturan N., Oturan M. A. (2007) Removal of methyl parathion from water by electrochemically generated Fenton's reagent. *Chemosphere*, 66, 841-848.
- 11.Zarei M., Niaei A., Salari D., Khataee A. R. (2010) Removal of four dyes from aqueous medium by the peroxi-coagulation method using carbon nanotube–PTFE cathode and neural network modelling*, J. Electroanal. Chem.*, 639, 167-174.
- 12. Daneshvar N., Hejazi M.J., Khataee A.R., Rangarangy B. (2004) Photocatalytic degradation of an organophosphorus pesticide phosalone in aqueous suspensions of titanium dioxide. *J. Environ. Heal. B.*, 39, 285-296.
- 13.Kurbus T., March Slokar Y., Majcen Le Marechal A., Voncinab D. B. (2003) The use of experimental design for the evaluation of the influence of variables on the H_2O_2 /UV treatment of model textile waste water. *Dyes and Pigments*, 58, 171-178.
- 14.Sun S. P., Li C. J., Sun J. H., Shi S. H., Fan M. H., Zhou Q. (2009) Decolorization of an azo dye Orange G in aqueous solution by Fenton oxidation process: Effect of system parameters and kinetic study. *J. Hazard. Mater.*, 161,1052-1057.
- 15.Gutowska A., Ka1uzna-Czaplinska J., Jozwiak W.K. (2007) Degradation mechanism of Reactive Orange 113 dye by H2O2/Fe2þ and ozone in aqueous solution. *Dyes and Pigments*,74, 41-46.
- 16.Kurbusa T., Slokara Y. M., Majcen Le Marechal A., Voncinab D. B. (2003)The use of experimental design for the evaluation of the influence of variables on the H_2O_2/UV treatment of model textile waste water*. Dyes and Pigments*, 58, 171-178.
- 17.Arau´ jo P.W., Brereton R.G. (1996) Experimental design II. Optimization. *Trends Anal. Chem*., 15, 63-70.
- 18.Brandvik P. J. (1998) Statistical simulation as an effective tool to evaluate and illustrate the advantage of experimental designs and response surface methods. *Chemomet. Intell. Lab. Syst.*, 42, 51-61.
- 19.Parida K.M., Sahu N., Biswal N.R., Naik B., Pradhan A.C. (2008) Preparation, characterization, and photocatalytic activity of sulfate-modified titania for degradation of methyl orange under visible light. *J. Iran. Chem. Soc.*, 318, 231-237.
- 20.Lau W. J., and Ismail A. F. (2010) Application of response surface methodology in pes/speek blend NF membrane for dyeing solution treatment. *Membrane Water Treatment*, 1, 49-60.
- 21.Daneshvar N., Salari D., Khataee A.R. (2003) Photocatalytic degradation of azo dye acid red 14 in water: investigation of the effect of operational parameters, *J. Photochem.Photobiol.*,157**,**111- 116.
- 22.Kincl M., Turk S., Vrecer F. (2005) Application of experimental design methodology in development and optimization of drug release method, *Int. J. Pharm*., 291, 39-49.

68

- 23.Zhang X., Wang R., Yang X., and Yu J. (2007) Central composite experimental design applied to the catalytic aromatization of isopherone to 3,5-xylenol. *Chemometr. Intell. Lab. Sys.*, 89, 45-50.
- 24.Avila A., Sanchez E.I., Gutierrez M.I. (2005) Optimal experimental design applied to the dehydrochlorination of poly(vinyl chloride), *Chemom. Intell. Lab. Syst.* 77, 247-250.
- 25.Gorji S., Bahram M. (2010) Experimental design for the study and optimization of the effect of different surfactants on the spectrophotometric determination of sulfide based on phenothiazine dye production. *Anal. Methods*, 2, 948-953.